**Customer Name** 

**Robby Martinez** 

Company

ICS

Quote is only valid for 30 days from the sized on date.

Location

Ventura, CA

Please reference Quote Number on all corresponding Purchase Orders

Quote #

Reference

Valve PSV/Tag Number

Quote Contact Linsey Allen SIZED ON

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ENG-1047000
2.19
15-Aug-19

MERCER VALVE CO., INC.®
"AUTO SEAT TECHNOLOGY"®

	GAS/VAPOR	DECLIBED CADACITY	Natural Cas		
	The state of the s	REQUIRED CAPACITY	**************************************	0.004	
	MOLECULAR WEIGHT			0.601	
	GAS COEFFICIENT COMPRESSIBILITY FACTOR	k-RATIO OF SPECIFIC HEATS		1.27	
	REQUIRED AREA	FLOW COEFFICIENT		0.818	
	LIQUID 1	REQUIRED CAPACITY	0.47 III-	0.818	
Fluid Data	SPECIFIC GRAVITY	DENSITY			
Fiulu Data	VISCOSITY	VISCOSITY CORRECTION FACTOR			
	REQUIRED AREA	FLOW COEFFICIENT			
	LIQUID 2	REQUIRED CAPACITY			
	SPECIFIC GRAVITY	DENSITY			
	VISCOSITY	VISCOSITY CORRECTION FACTOR			
	REQUIRED AREA	FLOW COEFFICIENT			
	SUPERIMPOSED CONST BP		0 psig	0 psig	
	BUILT-UP BP	TOTAL BACK PRESSURE		0 psig	
	OPERATING TEMP	RELIEVING TEMPERATURE	Set on Air  0.47 in²  9749.4 scfm  9749.4 scfm  7889 SCFM A  148.58 dB @ 100 ft  (5) - Carbon Steel / WCB  (T) - 15% GLASS FILLED PTFE  NO  STNLS STL  17-7 PH STNLS STL  316 STNLS STL  (1) - CLOSED CAP  9100 SERIES SPRING OPE  Threaded  91-34G51T3  2GX1T1U4  (34) - 1½" MNPT x 2" FNPT  A = 4.423 ± 0.062 in. (112.3442 ± 1.6 mm.) B :	70 °F	
	OPERATING PRESSURE	ATMOSPHERIC PRESSURE		14.696 psia	
Process Conditions	SET PRESSURE	CDTP		- Marco poss	
	OVER PRESSURE	INLET PRESSURE LOSSES		0 psig / 0 %	
		FLOWING PRESSURE		1114.696 psia	
	DISCHARGE COEFFICIENT AND AREAS	VALVE CERTIFICATION / DESIGN CODE	ASME Certified	ASME BPVC, SECTION VIII, DIVISION 1	
	SYSTEM TYPE		17.40  344.1  1.000  0.47 in²  0 psig  0 psig  70 °F  1000 psig  100 psig/10 %  ASME Certified As  Set on Air  0.47 in²  0.472 in²  9749.4 scf  7889 SCFM  148.58 dB @ 100 ft  (5) - Carbon Steel / WC  (T) - 15% GLASS FILLED PTFE  NO  STNLS STL  17-7 PH STNLS STL  316 STNLS STL  (1) - CLOSED CAP  9100 SERIES SPRING OF  Threaded  91-34G51T  2GX1T1L  (34) - 1½" MNPT x 2" FNPT  A = 4.423 ± 0.062 in. (112.3442 ± 1.6 mm.)  E -20°F to 400°F (-29°C to 204°C) 900	Blocked Flow	
	TOTAL REQUIRED AREA	Rupture Disk Correction	0.47 in <sup>2</sup>	1.0	
	SELECTED ORIFICE AREA SELECTED ORIFICE		0.472 in <sup>2</sup>	G ORIFICE	
2	MAXIMUM CAPACITY OF	GAS AT OVER PRESS.	9749.	4 scfm	
Sizing Results	MAXIMUM CAPACITY OF LIQUID 1 AT OVER PRESS.				
	The state of the s				
TAG	TAG CAPACITY				
	DECIBEL LEVEL	SINGLE OUTLET REACTION FORCE	148.58 dB @ 100 ft	597.95 lbf	
	INLET BASE / BODY N	1ATERIAL	(5) - Carbon Steel /	G ORIFICE  9749.4 scfm  889 SCFM AIR  597.95 lbf  Steel / WCB Carbon Steel  (1) - Fluorocarbon & BUNA N	
	SEAT	O-RINGS	1.000 ENT	(1) - Fluorocarbon & BUNA N	
Materials	SOUR SERVICE	TRIM MATERIALS	NO	(U) - 316 SS DISK & NOZZLE	
Materials	ADJ SCREW	ADJ BUSHING	STNLS STL	STNLS STL	
	SPRING	DISK	17-7 PH STNLS STL	316 STNLS STL	
	NOZZLE MATERIAL	NOZZLE TYPE	316 STNLS STL	Semi Nozzle	
	CAP TYPE	INLET PIPE TAP	(1) - CLOSED CAP	NO	
	Valve Type		9100 SERIES SPRING OPERATED VALVE		
	FLANGED OR THREADED		17.40 344.1 1.000 0.47 in²  0 psig 0 psig 70 °F  1000 psig 100 psig/10 %  ASME Certified Set on Air 0.47 in² 0.472 in² 9749.4  7889 SC 148.58 dB @ 100 ft (5) - Carbon Steel / (T) - 15% GLASS FILLED PTFE NO STNLS STL 17-7 PH STNLS STL 316 STNLS STL (1) - CLOSED CAP 9100 SERIES SPRING Threaded  91-34G5 2GX1 (34) - 1½" MNPT x 2" FNPT A = 4.423 ± 0.062 in. (112.3442 ± 1.6 mm.) -20°F to 400°F (-29°C to 204°C)		
	Valve P/N:			51T32U1	
Valve Information	Repair Kit P/N:		2GX1	T1U4	
	Inlet and Outlet		(34) - 11/2" MNPT x 2" FNPT		
	Center to Face Dimer	nsions	A = 4.423 ± 0.062 in. (112.3442 ± 1.6 mm.)	B = 2.312 ± 0.062 in. (58.7248 ± 1.6 mm	
	Valve Design Temp	Valve Design Pressure	1.000 0.47 in²  0 psig 0 psig 0 psig 70 °F  14  1000 psig 100 psig 100 psig/10 %  111  ASME Certified ASME BPVC, SE Set on Air Blo 0.47 in² 0.472 in² 0.472 in² G 9749.4 scfm  7889 SCFM AIR  148.58 dB @ 100 ft S: (5) - Carbon Steel / WCB Carbon Steel (T) - 15% GLASS FILLED PTFE (1) - Fluoro NO (U) - 316.5 STNLS STL SC 17-7 PH STNLS STL SE 17-7 PH STNLS STL SE 17-7 PH STNLS STL SE (1) - CLOSED CAP 9100 SERIES SPRING OPERATED VAL Threaded  91-34G51T32U1 2GX1T1U4  (34) - 1½" MNPT x 2" FNPT A = 4.423 ± 0.062 in. (112.3442 ± 1.6 mm.) B = 2.312 ± 0.06 900psig to 1200psig	900psig to 1200psig (6205.3kPag to 8273.7kPa	
Pricing Information	Quantity	Lead Time (ARO)	1		
montaction	Price Per Valve (US\$)	Total Valve Price (US\$)			

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Company

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Ventura, CA

Location Quote #

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Valve PSV/Tag Number

MERCER VALVE

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## MERCER VALVE CO., INC.®

			Page 2 o	"AUTO SEAT	"AUTO SEAT TECHNOLOGY"®	
Fluid Properties	Variable Name		Symbol	Input Value	<b>Equation Value</b>	
Gas	Molecular Weigh	it	M	17.4	17.4	
	Ratio of Specific	Heats	k	1.27	1.27	
	Compressibility		Z	1	1	
Process Conditions	Gas Required Are	ea	AGAS	0.47 in <sup>2</sup>	0.47 in2	
	Set Pressure		Pset	1000 psig	1000 psig	
	Over Pressure		Pover	10 %	100 psig	
	Inlet Line Loss		Ploss	0 %	0 psig	
	Variable Superimposed Back Pressure		Pvs	0 psig	0 psig	
	Constant Superimposed Back Pressure			O psig	0 psig	
	Built-up Back Pressure		Pbu	0 psig	0 psig	
	Atmospheric Pressure		Patm	14.696 psia	14.696 psia	
	Relieving Temperature		T1	70 °F	529.67 °R	
	Rupture Disk Correction		Кс	1	1	
	Noise Level Dista	nce	d	100 ft	100 ft	
Valve Data	Gas Discharge Co	efficient	KdGAS		0.818	
	Outlet Diameter		Do		1.939 in	
	Actual Valve Orifice Area		ATAG		0.472 in <sup>2</sup>	
	ASME Certified F	low Coefficient	KdTag		0.818	
Calculations	Symbol	Equation			<b>Equation Result</b>	
Flowing Pressure	P1	P1 = Pset + F	Pover - Ploss + Patm		1114.7 psia	
Total Back Pressure	P2	P2 = Pvs + P	cs + Pbu + Patm		14.696 psia	
Pressure Ratio	PR	PR = P1 / P2			75.9	
Critical Flow Nozzle Pre	20 1 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2		2/(k+1)]^[k/(k-1)]		614.43 psia	
Sonic Flow Verification			==> SONIC FLOW			
Gas Constant	С	C = 520 * { k	*[2/(k+1)]^[(k+1	)/(k-1)]}^0.5	344.1	

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Ventura, CA

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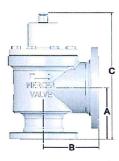
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Calculations	Symbol	Equation I	Equation Result
Total Required Area Selected Orifice	A	A = AGAS G ORIFICE	0.47 in <sup>2</sup> 0.472 in <sup>2</sup>
Tag Flowing Pressure	P1TAG	P1TAG = Pset + Povertag + Patm	1114.696 psia
Tag Capacity	VTAG	VTAG = 18.331 * A * P1TAG * KdTAG	7889 SCFM AIR
Maximum Gas Flow Rate Mass Flow	Vmax W	Vmax = 6.32 * C * KdGAS * P1 * Kc * A / ( T1 * Z * M ) ^ 0.5 W = Vmax * M / 6.32	9749.36 scfm 26841.59 lb/hr
Noise Level Calculations SoundPressureLevel Noise Level at 100 ft (30 m)	L L100	Calculated from Figure 18 in API 521 L100 = L + 10 * log ( 0.214967 * W * k *T1 / M )	95.1 dB 148.58 dB
Noise Level at distance d	Ld	Ld = L100 - 20 * log ( d / 100 )	148.58 dB
Reaction Forces Outlet Static Pressure Outlet Area	Po Ao	Po = Max Allowable Over Pressure $Ao = (\pi * Do ^2)/4$ $FGC = M / 2GC * (/// * T4) / (/// * 14) * Add / 2GC * (/// * T4) / (/// * 14) * Add / 2GC * (/// * T4) / (/// * 14) * Add / 2GC * (/// * T4) / (/// * 14) * Add / 2GC * (/// * T4) / (/// * 14) * Add / 2GC * (/// * T4) / (/// * 14) * Add / 2GC * (/// * T4) / (/// * 14) * Add / 2GC * (/// * T4) / (/// * 14) * Add / 2GC * (/// * T4) / (/// * 14) * Add / 2GC * (/// * T4) / (/// * 14) * Add / 2GC * (/// * T4) / (/// * 14) * Add / 2GC * (/// * T4) / (/// * 14) * Add / 2GC * (/// * T4) / (/// * 14) * Add / 2GC * (/// $	114.696 psia 2.953 in <sup>2</sup>
Gas Reaction Force for Open Discharge	FrGas	FrGas = W / 366 * { ( k * T1 ) / [ ( k + 1 ) * M ] } ^ 0.5 + [ ( Po - Patm ) * A	o] 597.95 lbf



Picture may not be representative of actual valve  $A = 4.423 \pm 0.062$  in. (112.3442  $\pm$  1.6 mm.)  $B = 2.312 \pm 0.062$  in. (58.7248  $\pm$  1.6 mm.)